

22510

12425

03 Hours / 70 Marks

Seat No.

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- Instructions –*
- (1) All Questions are *Compulsory*.
 - (2) Illustrate your answers with neat sketches wherever necessary.
 - (3) Figures to the right indicate full marks.
 - (4) Assume suitable data, if necessary.
 - (5) Use of Non-programmable Electronic Pocket Calculator is permissible.
 - (6) Mobile Phone, Pager and any other Electronic Communication devices are not permissible in Examination Hall.

Marks

- 1. Attempt any FIVE of the following:** **10**
- a) Define thermal conductivity and state It's S.I. Unit.
 - b) State and define two types of Convection.
 - c) Give the expression for Reynold's number and state it's significance.
 - d) State Kirchoff's law of Radiation.
 - e) Define condenser and cooler.
 - f) Define different types of condensation.
 - g) Define capacity and economy of an evaporator.

P.T.O.

- 2. Attempt any THREE of the following:** **12**
- a) State Fouriers Law of heat conduction. Give it's mathematical expression and state the terms used in it.
 - b) Give the Sider - Tate equation used to calculate the film coefficient in case of Laminar flow and Turbulent flow.
 - c) Draw neat labelled sketch of standard vertical tube evaporator.
 - d) Explain in brief the concept of black body.
- 3. Attempt any THREE of the following:** **12**
- a) Calculate the total heat loss by convection and radiation from an Unlagged steam pipe 50 mm B.d at 415 K to air at 290 K. Data - Take emissivity. $e = 0.9$. The film co-efficient for calculation is given by $hc = 1.18 (\Delta T/D_o)^{0.25} \text{ w/m}^2\text{k}$
 - b) Differentiate with sketch between parallel flow and counter current flow arrangement in Heat exchanger.
 - c) Explain construction and working of double pipe heat exchanger with diagram.
 - d) State Duhring's Rule. Explain boiling point elevation in Evaporation Operation.
- 4. Attempt any THREE of the following:** **12**
- a) Define emissivity, emissive power, black body and grey body.
 - b) Calculate the overall heat transfer coefficient if
 - i) Inside and outside, film heat transfer coeff are 12 and 11600 $\text{w}/(\text{m}^2.\text{k})$ respectively.
 - ii) Inside and outside diameters are 25 mm and 29 mm respectively.
 - iii) Thermal conductivity of pipe material is 34.9 $\text{w}/(\text{m.k})$
 - c) Derive the expression far rate of heat transfer by conducting through a plane wall.
 - d) Differentiate between dropwise and filmwise condensation. (Any four points.)
 - e) Compare forward feed and backward feed arrangements in case of multiple effect evaporator. (Any four points.)

5. Attempt any TWO of the following:**12**

- a) An evaporator operating at atmospheric pressure is fed at rate of 5000 kg/h of weak liquor containing 4% caustic soda. Thick liquor leaving the evaporator contains 25% caustic soda. Find the capacity of the evaporator.
- b) Derive the relationship $Q = UA \Delta T_{lm}$.
- c) A hot fluid enters a double pipe heat exchanger at a temperature of 423 K and to be cooled to 363 K by a cold fluid entering at 308 K and heated to 338 K. Shall they be directed in parallel flow or counter current flow to have a high rate of heat transfer.

6. Attempt any TWO of the following:**12**

- a) A furnace wall is constructed with 225 mm thick of fire brick, 120 mm of insulating brick and 225 mm of the building brick. The inside temperature is 1200 K and the outside temperature is 330 K. Find the heat loss per unit area and the temperature at the junction of the fire brick and insulating brick.

Data - K for fire, brick = 1.4 W/(m.k)

K for insulating brick = 0.2 W/(m.k)

K for building brick = 0.7 W/(m.k)

- b) Determine the heat transfer coefficient for water flowing in a tube of 16 mm diameter at a velocity of 3 m/s. The temperature of the tube is 297 K and the water enters at 353 K and leaves at 309 K. Using

i) Dittus - Bolter equation and

ii) Sieder - Tate equation

Data - Properties of water at mean bulk temp of 331 K are :

$\rho = 984.1 \text{ kg/m}^3$, $C_p = 4187 \text{ J/(K.kg)}$, $\mu = 485 \times 10^{-6} \text{ Pa.s}$,

$K = 0.657 \text{ W/(m.k)}$, viscosity of water at 297 K,

$\mu_w = 920 \times 10^{-6} \text{ Pa.s}$.

- c) Explain construction and working of Graphite block heat exchanger with neat sketch. Give its advantages.
