## WINTER - 2022 EXAMINATION

## Model Answer

## Subject Name: Fluid Mechanics and Machinery

Subject Code:

## Important Instructions to examiners:

1) The answers should be examined by key words and not as word-to-word as given in the model answer scheme.
2) The model answer and the answer written by candidate may vary but the examiner may try to assess the understanding level of the candidate.
3) The language errors such as grammatical, spelling errors should not be given more Importance (Not applicable for subject English and Communication Skills.
4) While assessing figures, examiner may give credit for principal components indicated in the figure. The figures drawn by candidate and model answer may vary. The examiner may give credit for any equivalent figure drawn.
5) Credits may be given step wise for numerical problems. In some cases, the assumed constant values may vary and there may be some difference in the candidate's answers and model answer.
6) In case of some questions credit may be given by judgement on part of examiner of relevant answer based on candidate's understanding.
7) For programming language papers, credit may be given to any other program based on equivalent concept.
8) As per the policy decision of Maharashtra State Government, teaching in English/Marathi and Bilingual (English + Marathi) medium is introduced at first year of AICTE diploma Programme from academic year 2021-2022. Hence if the students in first year (first and second semesters) write answers in Marathi or bilingual language (English +Marathi), the Examiner shall consider the same and assess the answer based on matching of concepts with model answer.

| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | $\begin{gathered} \text { Sub } \\ \text { Q. } \\ \text { N. } \end{gathered}$ | Answer | Marking <br> Scheme |
| :---: | :---: | :---: | :---: |
| Que. 1 |  | Attempt any FIVE of the following | 10 Marks |
|  | a) | Define fluid pressure intensity and pressure head. |  |
|  | Sol. | Pressure intensity: The force acting on the area in the normal direction is called as pressure Intensity. <br> Pressure head: Pressure head is defined as the vertical height or the free surface above any point in a fluid at rest. | 01 Mark for each definition |
|  | b) | Convert $10 \mathrm{~N} / \mathrm{cm}^{2}$ pressure in oil column of specific gravity 0.82 |  |
|  | Sol. | $\mathrm{P}=10 \mathrm{~N} / \mathrm{cm}^{2}=10 \times 10^{4} \mathrm{~N} / \mathrm{m}^{2}$ <br> Density of $\mathrm{Oil}=\rho_{\mathrm{o}}=0.82 \times 1000=820 \mathrm{~kg} / \mathrm{m}^{3}$ $\begin{aligned} \text { Pressure in oil column } & =H=P / W \\ & =P /\left(\rho_{o} \times g\right)=\left(10 \times 10^{4}\right) /(820 \times 9.81)=\mathbf{1 2 . 4 3} \mathbf{m} \text { of Oil } \end{aligned}$ | 01 Mark <br> 01 Mark |

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| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | $\begin{gathered} \hline \text { Sub } \\ \text { Q. } \\ \text { N. } \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  | c) | State the types of fluid flow. |  |
|  | Sol. | (i) Steady and Unsteady flow. <br> (ii) Uniform and Non-uniform flow. <br> (iii) Laminar and turbulent flow. <br> (iv) Rotational and Irrotational flow <br> (v) Compressible and incompressible flow. | $1 / 2$ mark <br> for each type |
|  | d) | State the various minor losses in the pipe. |  |
|  | Sol. | (i) Loss of head at Entry. <br> (ii) Loss of head at Exit. <br> (iii) Loss of head due to sudden enlargement. <br> (iv) Loss of head due to sudden contraction <br> (v) Loss of head due to sudden obstruction. <br> (vi) Loss of head due to bend or Elbow | 1/2 mark <br> for each loss |
|  | e) | Write Chezy's equation. State the meaning of each term. |  |
|  | Sol. | Chezy's formula, $\mathrm{V}=C \sqrt{m} i$ <br> Where; <br> $\mathrm{V}=$ velocity of water in pipe, <br> C = Chezy's constant, <br> $\mathrm{m}=$ hydraulic mean depth $=A / P=d / 4$ <br> $i=$ loss of head per unit length | 01 Mark <br> 01 Mark |
|  | f) | State the necessity of draft tube for every reaction turbine. |  |
|  | Sol. | (i) Draft tube permits a negative head to be established at the outlet of the runner and thereby increase the net head on the turbine. The turbine may be placed above the tail race without any loss of net head and hence turbine may be inspected properly. <br> (ii) Draft tube converts a large portion of the kinetic energy rejected at the outlet of the turbine into useful pressure energy. Without draft tube, the kinetic energy rejected at the outlet of the turbine will go waste to the tail race. <br> (iii) The net head on the turbine increases. <br> (iv) The turbine develops more power and also the efficiency of the turbine increases. | Any two 01 Mark for each |

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| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | $\begin{gathered} \hline \text { Sub } \\ \text { Q. } \\ \text { N. } \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  | g) | Define the following terms- <br> i) NPSH <br> ii) Negative Slip |  |
|  | Sol. | NPSH: The net positive suction head (NPSH) is defined as the absolute pressure head at the inlet of the pump to force the liquid into the pump at a given temperature. <br> Negative Slip: When theoretical discharge is less than actual discharge then the difference is called as negative slip. | 01 mark <br> 01 mark |
| Q. 2 |  | Attempt any THREE of the following: | 12 Marks |
|  | a) | Different pressure gauges shows following sets of reading <br> i) $100 \mathrm{kgf} / \mathrm{cm}^{2}$ <br> ii) $\mathbf{1 5}$ bar convert it into $\mathrm{N} / \mathrm{mm}^{2}$ and $\mathrm{N} / \mathrm{m}^{2}$ |  |
|  | Sol. | $\begin{aligned} & \text { i) } 100 \mathrm{kgf} / \mathrm{cm}^{2} \\ & \text { We know, } 1 \mathrm{Kg}=9.81 \mathrm{~N} \\ & 100 \mathrm{kgf} / \mathrm{cm}^{2}=100 \times 9.81=981 \mathrm{~N} / \mathrm{cm}^{2} \\ & 981 \mathrm{~N} / \mathrm{cm}^{2}=981 /\left(10^{2}\right)=9.81 \mathrm{~N} / \mathrm{mm}^{2} \\ & 9.81 \mathrm{~N} / \mathrm{mm}^{2}=9.81 /\left(10^{-3}\right)^{2}=9810 \times 10^{3} \mathrm{~N} / \mathrm{m}^{2} \\ & \text { ii) } 15 \mathrm{bar} \\ & 15 \mathrm{bar}=15 \times 10^{5} \mathrm{~N} / \mathrm{m}^{2} \\ & 15 \times 10^{5} \mathrm{~N} / \mathrm{m}^{2}=15 \times 10^{5} /\left(10^{3}\right)^{2}=1.5 \mathrm{~N} / \mathrm{mm}^{2} \end{aligned}$ | 01 mark <br> 01 mark <br> 01 mark <br> 01 mark |
|  | b) | A circular plate 3 m diameter is immersed in water is such a way that its greatest and least depth below the free surface of water are 4 m and 1 m respectively. Determine the total pressure and position of center of pressure. |  |
|  | Sol. | $d=3 \mathrm{~m}$ <br> greatest depth $=4 \mathrm{~m}$ <br> least depth $=1 \mathrm{~m}$ | 01 mark |

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| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | Sub <br> Q. <br> N. | Answer | Marking Scheme |
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|  |  | Here, Center of gravity, $\bar{X}=1+(3 / 2)=2.5 \mathrm{~m}$ $A=(\pi / 4) X d^{2}=(\pi / 4) X^{3} 2=7.068 \mathrm{~m}^{2}$ <br> Now, Total Pressure on circular Plate, $\mathbf{P}=\mathbf{W} \cdot \mathbf{A} \cdot \overline{\mathrm{X}}=9810 \times 7.068 \times 2.5=173357 \mathrm{~N}$ <br> Now, Position of center of Pressure $=I_{G} /(A \bar{X})+\bar{X}$ $\mathrm{I}_{\mathrm{G}}=(\pi / 64) \times \mathrm{d}^{4}=(\pi / 64) \times 3^{4}=3.976 \mathrm{~m}^{4}$ $\begin{aligned} \text { Position of center of Pressure } & =I_{G} /(\mathrm{A} \overline{\mathrm{X}})+\overline{\mathrm{X}} \\ & =3.976 /(7.068 \times 2.5)+2.5 \\ & =\mathbf{2 . 7 2 5} \mathbf{m} \end{aligned}$ | 01 mark <br> 01 mark <br> 01 mark |
|  | c) | Derive the equation for coefficient of discharge ( $\mathrm{C}_{\mathrm{d}}$ ) for Venturimeter. |  |
|  | Sol. |  | 01 mark |

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| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | $\begin{gathered} \text { Sub } \\ \text { Q. } \\ \mathrm{N.} \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  |  | Consider a venturimeter fitted in a horizontal pipe through which a fluid is flowing $\text { Let } \begin{aligned} \mathrm{P}_{1} & =\text { Pressure at section } 1 \\ \mathrm{~V}_{1} & =\text { Velocity at section } 1 \\ \mathrm{a}_{1} & =\text { Area at section } 1 \\ \mathrm{Z}_{1} & =\text { Datum head at section } 1 \end{aligned}$ <br> $P_{2}, V_{2}, a_{2}, Z_{2}$ are the corresponding value at section 2 <br> Assuming that is no loss of energy and apply Bernoulli's equation to section (1) and (2) $\frac{P_{1}}{w}+\frac{V_{1}^{2}}{2 g}+Z_{1}=\frac{P_{2}}{w}+\frac{V_{2}^{2}}{2 g}+Z_{2}$ <br> Since the meter is horizontal $\mathrm{Z}_{1}=\mathrm{Z}_{2}$ $\begin{aligned} \therefore \frac{P_{1}}{w}+\frac{V_{1}^{2}}{2 g} & =\frac{P_{2}}{w}+\frac{V_{2}^{2}}{2 g} \\ \frac{P_{1}-P_{2}}{w} & =\frac{V_{2}^{2}-V_{1}^{2}}{2 g} \end{aligned}$ <br> $\frac{P_{1}-P_{2}}{w}$ is the pressure head difference between section 1 and 2 , and it is denoted by h . $\therefore \quad \mathrm{h}=\frac{\mathrm{V}_{2}^{2}-\mathrm{V}_{1}^{2}}{2 \mathrm{~g}}$ <br> Now applving continuity equation, $\begin{aligned} \mathrm{Q} & =\mathrm{a}_{1} \mathrm{~V}_{1}=\mathrm{a}_{2} \mathrm{~V}_{2} \\ \mathrm{~V}_{1} & =\left(\frac{\mathrm{a}_{2}}{\mathrm{a}_{1}}\right) \mathrm{V}_{2} \end{aligned}$ | 01 mark |

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| $\begin{aligned} & \text { Q. } \\ & \text { No } \end{aligned}$ | $\begin{array}{\|l\|} \hline \text { Su } \\ \text { b } \\ \text { Q. } \\ \mathrm{N} . \end{array}$ | Answer | Markin <br> g <br> Scheme |
| :---: | :---: | :---: | :---: |
|  |  | $\begin{aligned} \therefore \quad \mathrm{h} & =\frac{\mathrm{V}_{2}^{2}-\left(\mathrm{a}_{2} / \mathrm{a}_{1}\right)^{2} \mathrm{~V}_{2}^{2}}{2 \mathrm{~g}} \\ & =\frac{\mathrm{V}_{2}^{2}}{2 \mathrm{~g}}\left[1-\left(\frac{\mathrm{a}_{2}}{\mathrm{a}_{1}}\right)^{2}\right] \\ \mathrm{h} & =\frac{\mathrm{V}_{2}^{2}}{2 \mathrm{~g}}\left(\frac{\mathrm{a}_{1}^{2}-\mathrm{a}_{2}^{2}}{\mathrm{a}_{1}^{2}}\right) \\ \mathrm{v}^{2} & =\frac{\mathrm{a}_{1}^{2}(2 \mathrm{gh})}{\left(\mathrm{a}_{1}^{2}-\mathrm{a}_{2}^{2}\right)} \\ \mathrm{V}_{2} & =\frac{\mathrm{a}_{1} \sqrt{2 \mathrm{gh}}}{\sqrt{\mathrm{a}_{1}^{2}-\mathrm{a}_{2}^{2}}} \end{aligned}$ <br> Discharge through venturimeter $\begin{aligned} & \mathbf{Q =} \mathbf{V}_{2} \mathbf{a}_{2} \\ & \\ & \quad \mathbf{Q}=\frac{\mathrm{a}_{1} \mathrm{a}_{2} \sqrt{2 \mathrm{gh}}}{\sqrt{\mathrm{a}_{1}^{2}-\mathrm{a}_{2}^{2}}} \end{aligned}$ <br> This is the discharge under ideal condition, called as theoretical discharge. $\left.\begin{array}{rl} \text { but Actual discharge }= & \text { Coefficient of discharge } \\ & \times \text { Theoretical discharge } \end{array}\right\} \begin{aligned} \mathbf{Q}= & \mathbf{C}_{\mathbf{d}} \frac{\mathbf{a}_{1} \mathbf{a}_{2} \sqrt{2 \mathbf{g h}}}{\sqrt{\mathbf{a}_{1}^{2}-\mathbf{a}_{2}^{2}}} \\ \text { Where } \quad \mathbf{C}_{\mathrm{d}}= & \text { coefficient of discharge } \end{aligned}$ | 01 mark |

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| $\begin{gathered} \text { Q. } \\ \text { No. } \end{gathered}$ | $\begin{gathered} \hline \hline \text { Sub } \\ \text { Q. } \\ \mathrm{N} . \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  | d) | Explain with sketch the procedure for measuring velocity in pipe using Pitot tube. |  |
|  | Sol. | - Pitot tube is used for measuring the local velocity of flow at any point in a pipe or channel. <br> - Its working principle is if velocity of flow at a point becomes zero, there is increase in pressure energy. <br> - In its simplest form, it is a glass tube bent at right angle as shown in fig. <br> - The lower end is bend through $90^{\circ}$ is facing the upstream direction. The liquid rises up in the tube due to the conversion of kinetic energy into pressure energy. <br> - Piezometer tube gives pressure head and pitot tube gives pressure and velocity head. <br> - The velocity is determined by measuring the rise (h) of liquid in the tube as shown in fig. <br> Actual velocity $=\mathrm{V}=$ $C_{v} \sqrt{2 g h}$ <br> - The bent end of pitot tube should be facing the direction of flow of liquid otherwise there will error in calculation. | 01 Mark <br> 01 Mark <br> 01 Mark <br> 01 Mark |
| Que. 3 |  | Attempt any THREE of the following | 12 Marks |
|  | a) | A Venturimeter is installed in a pipeline of 30 cm diameter, the difference of pressure at entrance and throat read by mercury manometer is 5 cm . When the water flows at a rate of $0.05 \mathrm{~m}^{3} / \mathrm{sec}$. If the discharge coefficient of meter is 0.96 determine the diameter of throat |  |

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| $\begin{gathered} \text { Q. } \\ \text { No. } \end{gathered}$ | Sub <br> Q. <br> N. | Answer | Marking Scheme |
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|  | Sol. | Sain. Given data <br> - Diameter at inlet $d_{1}=30 \mathrm{~cm}=0.3 \mathrm{~m}$ <br> - Difference of mercury level $x=5 \mathrm{~cm}=0.05 \mathrm{~m}$ <br> - Fiow Rate $Q=0.05 \mathrm{~m}^{3} / \mathrm{sec}$ <br> - Coeff. of discharge $C d=0.96$ <br> - Diameter of throat $d_{2}=$ ? <br> - Spec. gravity of mercury $S_{m}=13.6$ <br> - Spe. Gravity of water $S w=1$ <br> 1) Area at inlet $\therefore \quad a_{1}=\frac{\pi}{4}\left(d_{1}\right)^{2}=\frac{\pi}{4}(0.3)^{2}$ $a_{1}=0.0706 \mathrm{~m}^{2}$ <br> 2) Pressure head $\begin{aligned} & \text { essure head } \\ & \therefore \text { Pressure difference } \begin{aligned} h & =x\left(\frac{S_{m}}{S w 1}-1\right) . \\ & =0.05\left(\frac{13.6}{1}-1\right) \\ h & =0.63 \mathrm{~m} \end{aligned} \end{aligned}$ <br> 3) For venturimeter $\begin{aligned} & \therefore Q=\frac{c d \cdot a_{1} \cdot a_{2} \cdot \sqrt{2 g n}}{\sqrt{a_{1}{ }^{2}-a_{2}{ }^{2}}} \\ & \therefore 0.05=\frac{0.96 \times 0.0706 \times a_{2} \times \sqrt{2 \times 9.81 \times 0.63}}{\sqrt{(0.0706)^{2}-\left(a_{2}\right)^{2}}} \\ & \sqrt{(0.0706)^{2}-\left(a_{2}\right)^{2}}=4.76 a_{2} \end{aligned}$ <br> squaring on both side $\begin{aligned} & (0.0706)^{2}-\left(a_{2}\right)^{2}=\left(4.76 \times a_{2}\right)^{2} \\ & \therefore \\ & \therefore .98 \times 10^{-3}=22.65 a_{2}^{2}+a_{2}^{2} \\ & \therefore \\ & 4.98 \times 10^{-3}=23.65 a_{2}^{2} \\ & \therefore \\ & a_{2}^{2}=2.10 \times 10^{-4} \\ & \\ & a_{2}=0.01449 \end{aligned}$ <br> We know that $\begin{gathered} a_{2}=\frac{\pi}{4} d_{2}^{2} \\ \therefore 0.01449=\frac{\pi}{4} d_{2}^{2} \\ d_{2}^{2}=0.01844 \\ \therefore d_{2}=0.1358 \mathrm{~m} \end{gathered}$ <br> $\therefore$ Diameter of throat $d_{2}=13.58 \mathrm{~cm}$ | 01 Mark <br> 01 Mark |

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| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | Sub <br> Q. <br> N. | Answer | Marking Scheme |
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|  | b) | Explain H.G.L. and T.E.L. with neat sketch. |  |
|  | Sol. | Hydraulic gradient line (HGL) :- <br> Hydraulic gradient line is basically defined as the line which will give the sum of pressure head and datum head or potential head of a fluid flowing through a pipe with respect to some reference line. <br> Hydraulic gradient line= $P / w+z$ <br> Total Energy Line (TEL):- <br> Total energy line is basically defined as the line which will give the sum of pressure head, potential head and kinetic head of a fluid flowing through a pipe with respect to some reference line. $\text { Total Energy Line }=v^{2} / 2 g+P / w+z$ | 01 Mark <br> 01 Mark <br> 02 Mark |
|  | c) | State the equation for hydraulic power transmission through pipe and obtain the condition for maximum power transmission. |  |
|  | Sol. | Power transmitted through pipe <br> $P=$ (weight of liquid flowing per second) $\times$ ( Outlet Head) $\mathrm{P}=\mathrm{w} \times \mathrm{Q} \times\left(\mathrm{H}-\mathrm{h}_{\mathrm{f}}\right)$ <br> Condition for maximum power transmission through the pipe:- <br> Differentiate the above equation w.r.t. velocity ' $v$ ' and equate with zero | 01 Mark |

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| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | $\begin{gathered} \hline \text { Sub } \\ \text { Q. } \\ \mathrm{N} . \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  |  | $\begin{array}{cc}  & \frac{d(P o w e r)}{d V}=0 \\ & \frac{d}{d V}[W Q(H-h F)]=0 \\ \therefore & \frac{d}{d V}\left[W \cdot Q\left(H-\frac{4 F l V^{2}}{2 g d}\right)\right]=0 \\ \therefore & \frac{d}{d v}\left[\left(W \cdot \frac{\pi}{4} d^{2} V\right) \cdot\left(H-\frac{4 F R V^{2}}{2 g d}\right)\right]=0 \\ \therefore & \frac{d}{d V}\left[\left(W \cdot \frac{\pi}{4} d^{2}\right) \cdot\left(H \cdot v-\frac{4 F R V^{3}}{2 g d}\right)\right]=0 \\ \therefore & W \cdot \frac{\pi}{4} d^{2} \frac{d}{d V}\left[H \cdot V-\frac{4 F R V^{3}}{2 g d}\right]=0 \\ \therefore & H-\frac{\pi}{4} d^{2}\left[H-\frac{4 \times 3 F l V^{2}}{2 g d}\right]=0 \\ \therefore & H-3 h F=0 \\ \therefore & H=3 h F \\ \therefore & H=0 \\ \therefore & H F=\frac{4}{2 g} \end{array}$ | 01 Mark <br> 01 Mark <br> 01 Mark |
|  | d) | Derive an expression for force exerted by jet on stationary inclined flat plate in direction of jet. |  |
|  | Sol. | Fig. Impact of jet on an inclined fixed plate | 01 Mark |

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| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | $\begin{gathered} \hline \hline \text { Sub } \\ \text { Q. } \\ \mathrm{N} . \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  |  | Let, $\begin{aligned} & d=\text { diameter of jet } \\ & a=\text { Area of jet }=(\pi / 4) d^{2} \\ & V=\text { Velocity of jet before striking the plate } \\ & V \sin \theta=\text { component of velocity normal to plate } \\ & m=\text { mass of water striking the plate per sec in } \mathrm{Kg} . \\ & m=\rho a V \end{aligned}$ <br> Fn = Normal force on the plate. <br> $\mathrm{Fn}=$ mass of water X (velocity before impact in the direction normal to plate - Velocity after impact in the direction normal to plate ) $\begin{aligned} F n & =\rho a V(V \sin \theta-0) \\ & =\rho a V^{2} \sin \theta \end{aligned}$ <br> $\mathrm{Fx}=$ Force in the direction of jet, $\quad \mathrm{Fx}==\mathrm{Fn} \sin \theta=\rho \mathrm{aV}^{2} \sin ^{2} \theta$ | 01 Mark <br> 01 Mark <br> 01 Mark |
|  | e) | A horizontal jet of water is delivered under an effective head of 25 m . Calculate the diameter of jet if the force exerted by the jet on a vertical fixed plate is 2.22 kN . Take coefficient of velocity as 0.99 |  |
|  | Sol. | - Given data. <br> effective head $\begin{aligned} h & =25 \mathrm{~m} \\ \text { Force } F & =2.22 \mathrm{KN}=2.22 \times 10^{3} \mathrm{~N} .\end{aligned}$ $\begin{aligned} & =2.22 \mathrm{KN}=2.22 \\ & 10 \text { city } C_{V}=0.99 \end{aligned}$ <br> Coefficient of velocity $C_{V}=0.99$ mass density of water $\rho=1000 \mathrm{~kg} / \mathrm{m}^{3}$ <br> Dlameter of jet $d=$ ? <br> $\therefore$ velocity of jet $\begin{aligned} v & =C_{v} \sqrt{2 g h} \\ & =0.99 \sqrt{2 \times 9.81 \times 25} \\ v & =21.93 \mathrm{~m} / \mathrm{sec} \end{aligned}$ | 01 Mark |


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| $\begin{gathered} \mathrm{Q} . \\ \text { No. } \end{gathered}$ | $\begin{gathered} \text { Sub } \\ \text { Q. } \\ \text { N. } \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  | b) | Classify turbines according to following: <br> i) Head at the inlet of turbine <br> ii) The direction of flow of water through runner |  |
|  | Sol. | According to the head available at inlet to the turbine <br> 1) Low head turbine ( 2 m to 15 m ) eg. Kaplan turbine <br> 2) Medium head turbine ( 16 m to 70 m ) eg. Francis turbine <br> 3) High head turbine ( 71 m and above) eg. Pelton wheel turbine <br> According to the direction of flow of water through runner: - <br> 1) Tangential flow turbine eg. Pelton wheel turbine <br> 2) Radial flow turbine eg. Inward flow and outward flow turbine. <br> 3) Axial flow turbine eg. Kaplan turbine <br> 4) Mixed flow turbine eg Modern Francis turbine | 02 Mark <br> 02 Mark |
|  | c) | A pelton wheel bucket is $1 \mathbf{m}$ in diameter. Pressure head at nozzle when it is closed is 15 bar. The discharge when nozzle is open is $3.5 \mathrm{~m}^{3} / \mathrm{min}$. If speed is 600 RPM , Calculate power developed and hydraulic efficiency. |  |
|  | Sol. | Soln. Given data. <br> Diameter of bucket $D=1 \mathrm{~m}$ <br> Pressure at nozzle $P=15$ bar $=15 \times 10^{5} \mathrm{~N} / \mathrm{m}^{2}$ <br> Discharge $Q=3.5 \mathrm{~m}^{3} / \mathrm{min}=0.058 \mathrm{~m}^{3} / \mathrm{sec}$ <br> Turbine speed $N=600 \mathrm{rpm}$ <br> Power $P=$ ? $\eta_{\text {nyd }}=?$ <br> Let $C V=0.98$, $\eta_{\text {overall }}=85 \%$ <br> 1) Pressure head <br> (student may assume $c v=1, \eta_{\text {overall }}=100 \%$ ) $\begin{aligned} & H=\frac{p}{\omega}=\frac{15 \times 10^{5}}{9810} \\ & H=152.9 \mathrm{~m} \end{aligned}$ <br> 2) velocity of jet $\begin{aligned} v & =C_{v} \times \sqrt{2 g H} \\ & =0.98 \times \sqrt{2 \times 9.81 \times 152.9} \\ v & =53.67 \mathrm{~m} / \mathrm{s} \end{aligned}$ | Find <br> $\mathrm{H}, \mathrm{v}, \mathrm{u}$ <br> 02 Mark |


| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | $\begin{gathered} \text { Sub } \\ \text { Q. } \\ \mathrm{N} . \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  |  | 3) Tangential velocity $\begin{aligned} & u=\frac{\Pi D N}{60}=\frac{\Pi \times 1 \times 600}{60} \\ & u=31.41 \mathrm{~m} / \mathrm{s} \end{aligned}$ <br> 4) Power developed $\begin{aligned} & \eta_{\text {overall }}=\frac{P}{\omega \cdot Q H} \\ & \therefore P=\eta_{\text {overall }} \times \omega \cdot Q H \\ &=0.85 \times 9810 \times 0.058 \times 152.9 \\ &=73.94 \times 10^{3} \text { Watt } \\ & P=73.94 \mathrm{~kW} \end{aligned}$ <br> 5) Hydraulic efficiency $\begin{aligned} & \eta_{\text {hyd }}=\frac{2 u(v-u)(1+\cos \phi)}{v^{2}} \quad\left(\text { But } \phi=0^{\circ}\right) \cos \phi=1 \\ & \cos 0=1 \\ &=\frac{2 \times 31.41(53.67-31.41)(1+1)}{(53.67)^{2}} \\ &=\frac{2796.74}{2880.46} \\ & \eta_{\text {hyd }}=0.9709 \\ & \% \eta_{\text {hyd }}=97.09 \% \end{aligned}$ | 01 Mark <br> 01 Mark |
|  | d) | Define the following w.r.t. centrifugal pump. <br> i) Manometric head ii) Manometric efficiency |  |
|  | Sol. | Manometric Head :- It is the total head that pump is required to develop. This includes all losses. This is equal to difference between pressure head at inlet \& outlet of pump. $\mathrm{Hm}=\mathrm{h}_{\mathrm{s}}+\mathrm{h}_{\mathrm{d}}+\mathrm{h}_{\mathrm{fs}}+\mathrm{h}_{\mathrm{fd}}+\mathrm{v}_{\mathrm{d}} / 2 \mathrm{~g}$ <br> Manometric Efficiency :- It is define as a ratio of the manometric head to the work done by impeller per newton of flowing water. <br> $\eta_{\text {mano }}=\frac{\text { Manometric Head }}{\text { Work done by Impeller }}$ <br> $\eta_{\text {mano }}=\frac{H_{m}}{\frac{V_{w 1} u_{1}}{g}}$ | 02 Mark <br> 02 Mark |
|  |  | Page No: |  |

$\left.\begin{array}{|l|l|l|l|l|}\hline \begin{array}{c}\text { Q. } \\ \text { No. } \\ \text { Q. } \\ \text { N. }\end{array} & \text { Answer } & \begin{array}{l}\text { Marking } \\ \text { Scheme }\end{array} \\ \hline & \text { e) } & \text { Explain the working of double acting Reciprocating pump with neat sketch. }\end{array}\right]$
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| $\begin{aligned} & \text { Q. } \\ & \text { No. } \end{aligned}$ | Sub <br> Q. <br> N. | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  | Sol. | Diameter of pipe, $\mathrm{d}=0.3 \mathrm{~m}$ <br> Total head $=0.25 \mathrm{~m}$ <br> Static head $=0.2$ <br> Dynamic Head $=0.25-0.2=0.05 \mathrm{~m} / \mathrm{sec}$ <br> Mean velocity $=0.78$ Central Velocity <br> Coefficient of velocity, $\mathrm{C}_{\mathrm{v}}=0.98$ <br> Central Velocity $=\mathrm{C}_{\mathrm{v}} \sqrt{2 g h}=0.98 \sqrt{2 X 9.81 X 0.05}=0.97 \mathrm{~m} / \mathrm{sec}$ <br> Mean velocity $=0.78 \times 0.97=0.7566 \mathrm{~m} / \mathrm{sec}$ <br> Discharge, $Q=$ Area of pipe $X$ Mean velocity $Q=\frac{\pi}{4} d^{2} X \text { Mean Velocity }=\frac{\pi}{4}(0.3)^{2} \times 0.7566=0.05348 \mathrm{~m}^{3} / \text { sec }$ <br> Quantity of water in lit/sec=0.05348X $1000=53.48 \mathrm{lps}$ | 01 Mark <br> 01 Mark <br> 01 Mark <br> 01 Mark <br> 01 Mark <br> 01 Mark |
|  | b) | Find the maximum power that can be transmitted by a power station through a hydraulic pipe 3 Km long and 0.2 m diameter. The pressure at the power station is 60 bars. Take $\mathrm{f}=0.0075$ |  |
|  | Sol. | Length of pipe, $\mathrm{L}=3 \mathrm{~km}=3000 \mathrm{~m}$ <br> Diameter of pipe, $\mathrm{D}=0.2 \mathrm{~m}$ <br> Coefficient of friction, $\mathrm{f}=0.0075$ <br> Pressure at power station, $\mathrm{P}=60 \mathrm{bar}=60 \times 10^{5} \mathrm{~N} / \mathrm{m}^{2}$ $\begin{aligned} & \mathrm{H}=\frac{P}{w}=\frac{60 \times 10^{5}}{9810}=611 \mathrm{~m} \quad h_{f}=\frac{H}{3}=\frac{611}{3}=203.66 \mathrm{~m} \\ & h_{f}=\frac{4 f l V^{2}}{2 g d}=\frac{4 \times 0.075 \times 3000 V^{2}}{2 \times 9.81 \times 0.2}=229.35 \mathrm{~V}^{2} \\ & 203.66=229.35 \mathrm{~V}^{2}, \quad \mathrm{v}^{2}=0.8879 \end{aligned}$ $V=0.9422 \mathrm{~m} / \mathrm{sec}$ <br> Discharge, $\mathrm{Q}=\mathrm{V} \times$ Area $=\mathbf{0 . 9 4 2 2} \times \frac{\pi}{4} d^{2}=0.9422 \times \frac{\pi}{4}(0.2)^{2}=0.0296 \mathrm{~m}^{3} / \mathrm{sec}$ <br> Head available at outlet of pipe $=H-h_{f}=611-203.66=407.34 \mathrm{~m}$ <br> Maximum power available $=\frac{\rho g Q \times \text { Head at outlet of pipe }}{1000} K w$ <br> Maximum power available $=\frac{1000 \times 9.81 \times 0.0296 \times 407.34}{1000}=118.28 \mathrm{kw}$ | 01 Mark <br> 01 Mark <br> 01 Mark <br> 01 Mark <br> 01 Mark <br> 01 Mark |

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| $\begin{gathered} \text { Q. } \\ \text { No. } \end{gathered}$ | $\begin{gathered} \text { Sub } \\ \text { Q. } \\ \text { N. } \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  | c) | A jet of water 80 mm diameter moving with a velocity $\mathbf{2 0 ~ m / s e c , ~ s t r i k e s ~ a ~ s t a t i o n a r y ~}$ plate. Find the normal force on the palate, when <br> i) The plate is normal to the jet <br> ii) The angle between jet and plate is $30^{\circ}$ |  |
|  | Sol. | Case 1) Force exerted by the jet of water on stationary vertical flat plate <br> $V=$ Velocity of jet $=20 \mathrm{~m} / \mathrm{sec} \quad d=$ Diameter of jet $=80 \mathrm{~mm}=0.80 \mathrm{~m}$ <br> $\mathrm{a}=\mathrm{C} /$ S Area of jet $=\frac{\pi}{4} d^{2}=\frac{\pi}{4}(0.8)^{2}=0.5024 \mathrm{~m}^{2}$ <br> Force exerted by the jet on stationary vertical flat plate in the direction of jet, $\mathrm{F}_{\mathrm{x}}=\rho a \mathrm{~V}^{2}=1000 \times 0.5024 \times\left(20^{2}\right)=200960 \mathrm{~N}$ <br> Force exerted by the jet of water on stationary inclined flat plate <br> $V=$ Velocity of jet $=20 \mathrm{~m} / \mathrm{sec}, \quad d=$ Diameter of jet $=80 \mathrm{~mm}=0.80 \mathrm{~m}$ <br> $\mathrm{a}=\mathrm{C} /$ S Area of jet $=\frac{\pi}{4} d^{2}=\frac{\pi}{4}(0.8)^{2}=0.5024 \mathrm{~m}^{2}$, <br> $\theta=$ Angle between jet and plate $=30^{\circ}$ <br> Force exerted by the jet on stationary vertical flat plate in normal direction to plate, $F_{n}=\rho \text { a } V^{2} \sin \theta=1000 \times 0.5024 \times\left(20^{2}\right) \operatorname{Sin}(30)=100480 \mathrm{~N}$ | 01 Mark <br> 02 Mark <br> 01 Mark <br> 02 Mark |

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| Que.6 |  | Attempt any TWO of the following | 12 Marks |
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|  | a) | Explain the construction and working principle of Pelton wheel turbine with neat sketch. |  |

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| $\mathbf{Q} .$ <br> No. | $\begin{gathered} \text { Sub } \\ \text { Q. } \\ \text { N. } \end{gathered}$ | Answer | Marking Scheme |
| :---: | :---: | :---: | :---: |
|  | b) | A centrifugal pump is to discharge water at the rate of 110 lit/sec at the speed of 1450 rpm against head of 13 m . Impeller diameter is $\mathbf{2 5 0 ~ \mathrm { mm }}$ and its width is 50 mm . If manometric efficiency is $75 \%$, determine=ne Vane angle at outer periphery. |  |
|  | Sol. | Discharge $\mathrm{Q}=110 \mathrm{lit} / \mathrm{sec}=0.110 \mathrm{~m}^{3} / \mathrm{sec}$ <br> Speed $\mathrm{N}=1450 \mathrm{rpm}$ <br> Manometric head $H_{\text {mano }}=13 \mathrm{~m}$ <br> Impeller Diameter at outlet $\mathrm{D}_{2}=250 \mathrm{~mm}=0.250 \mathrm{~m}$ <br> Width at outlet $\mathrm{B}_{2}=50 \mathrm{~mm}=0.050 \mathrm{~m}$ <br> Manometric Efficiency $\eta_{\text {Mano }}=0.75$ <br> Vane angle at outlet of periphery, $\phi$ <br> Tangential velocity of impeller at outlet $=\mathrm{u}_{2}=\frac{\pi D_{2} N}{60}=\frac{\pi \times 0.25 \times 1450}{60}=18.98 \mathrm{~m} / \mathrm{sec}$ <br> Discharge, $\mathrm{Q}=\pi D_{2} B_{2} \mathrm{X} \mathrm{V}_{\mathrm{f} 2}$ $\mathrm{V}_{\mathrm{f} 2}=\frac{Q}{\pi D_{2} B_{2}}=\frac{0.110}{\pi x 0.25 \times 0.05} 3.0 \mathrm{~m} / \mathrm{sec}$ <br> Manometric Efficiency $\eta_{\text {Mano }}=\frac{g H_{\text {mano }}}{V_{w 2} u_{2}}$ $\begin{gathered} 0.75=\frac{9.81 \times 13}{V_{w 2} \times 18.98} \\ V_{w 2}=8.9589 \mathrm{~m} / \mathrm{sec} \end{gathered}$ <br> From velocity triangle at outlet, $\begin{aligned} & \tan \phi=\frac{V_{f 2}}{u_{2-} V_{w 2}}=\frac{3.0}{18.98-8.9589}=0.299 \\ & \phi=16.64^{\circ} \end{aligned}$ | 01 Mark <br> 02 Mark <br> 01 Mark <br> 01 Mark <br> 01 Mark |

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\begin{array}{|l|c|l|l|}\hline \begin{array}{l}\text { Q. } \\
\text { No. }\end{array} & \begin{array}{c}\text { Sub } \\
\text { Q. } \\
\text { N. }\end{array} & & \begin{array}{l}\text { Marking } \\
\text { Scheme }\end{array}
$$ <br>

\hline \& c) \& Centrifugal pump not delivering water, give at least three reasons and remedies.\end{array}\right]\)| Any 03 |
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